



From Medium-Deep Geothermal to District Heating: Thermo-Economic Assessment of Different Heat Pump Configurations

Isabella Elbe, Arianna Passamonti, Hartmut Sliethoff, Christopher Schiffler

Chair of Energy Systems, Technical University of Munich

Motivation

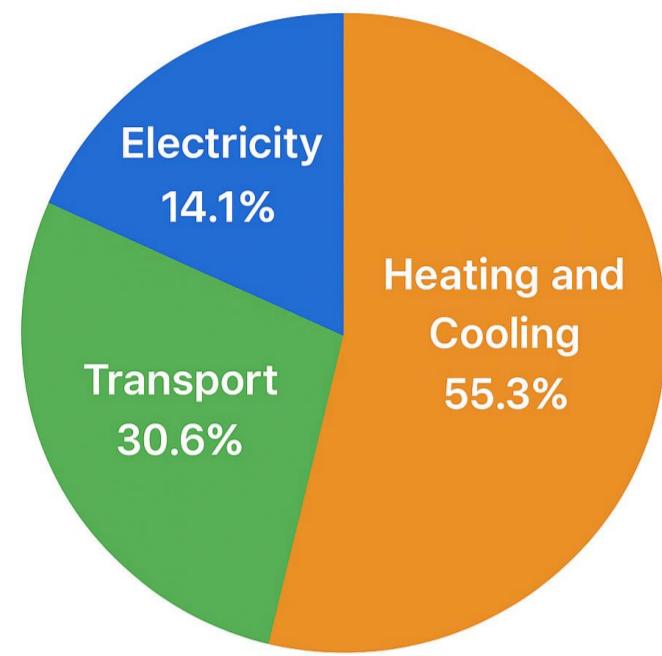


Figure 1: Energy consumption by sector in Germany in 2024¹

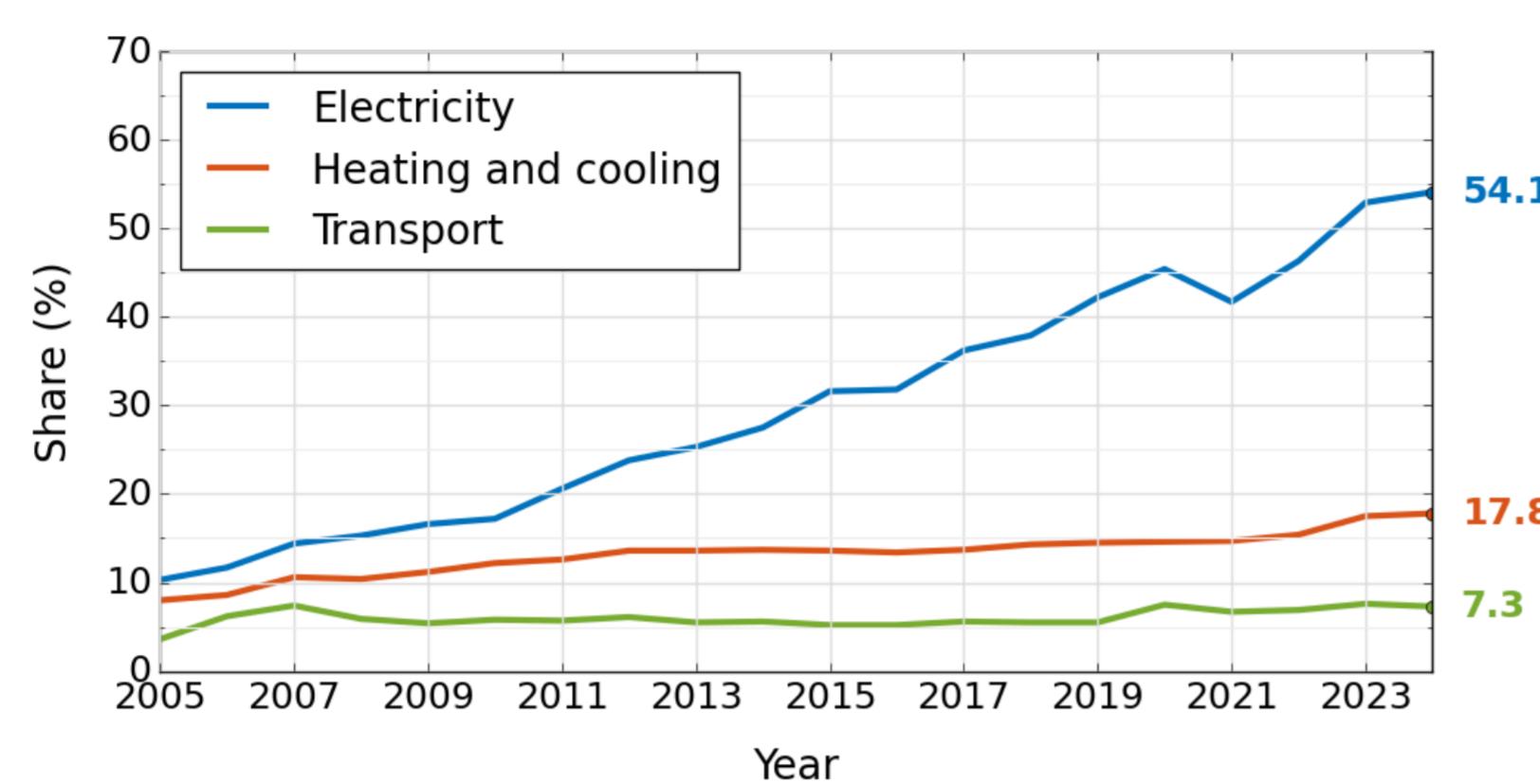


Figure 2: Share of renewable energy sources per sector in Germany¹

- Heating and cooling sector dominates consumption
- Heating sector remains largely fossil-based
- High and growing share of renewables in electricity

→ Decarbonizing Heating sector is of big interest → High promise to decarbonize district heating with large-scale heat pumps

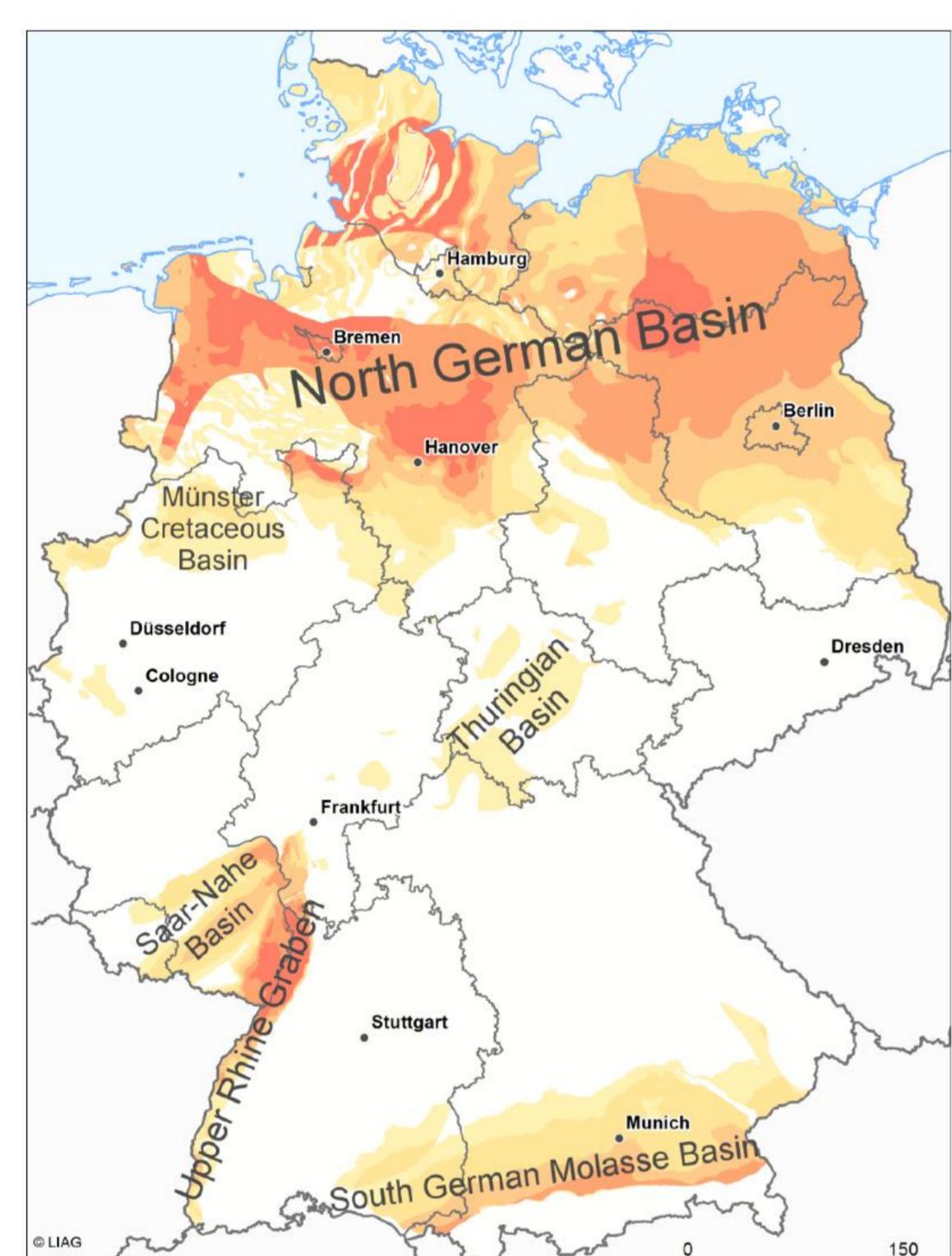


Figure 3: German regions with hydrothermal resources and associated temperature ranges³

- Deep-geothermal sources (>100°C) can be used directly for District Heating Systems (DHS) → potential limited to selected regions
- E.g. only 40% of Bavaria's heat demand could be covered with deep-geothermal-technologie²
- Significant medium-deep geothermal potential (<100°C) in Germany
- Large-scale heat pumps are required to utilize medium-deep resources for conventional DHS
- Optimal design and operational concepts are pivotal to achieve competitive economics

Methodology

Real Data

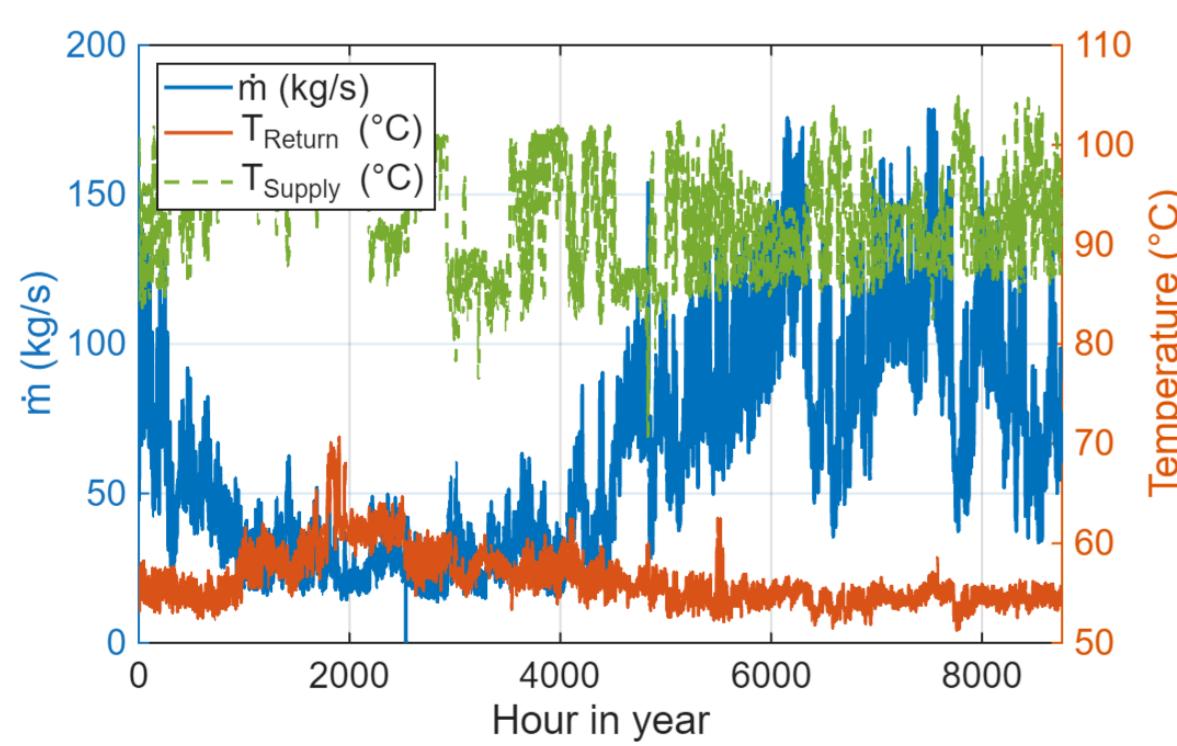


Figure 6: District Heating Network Data from geothermal plant in Pullach, Germany

Off-Design Simulation

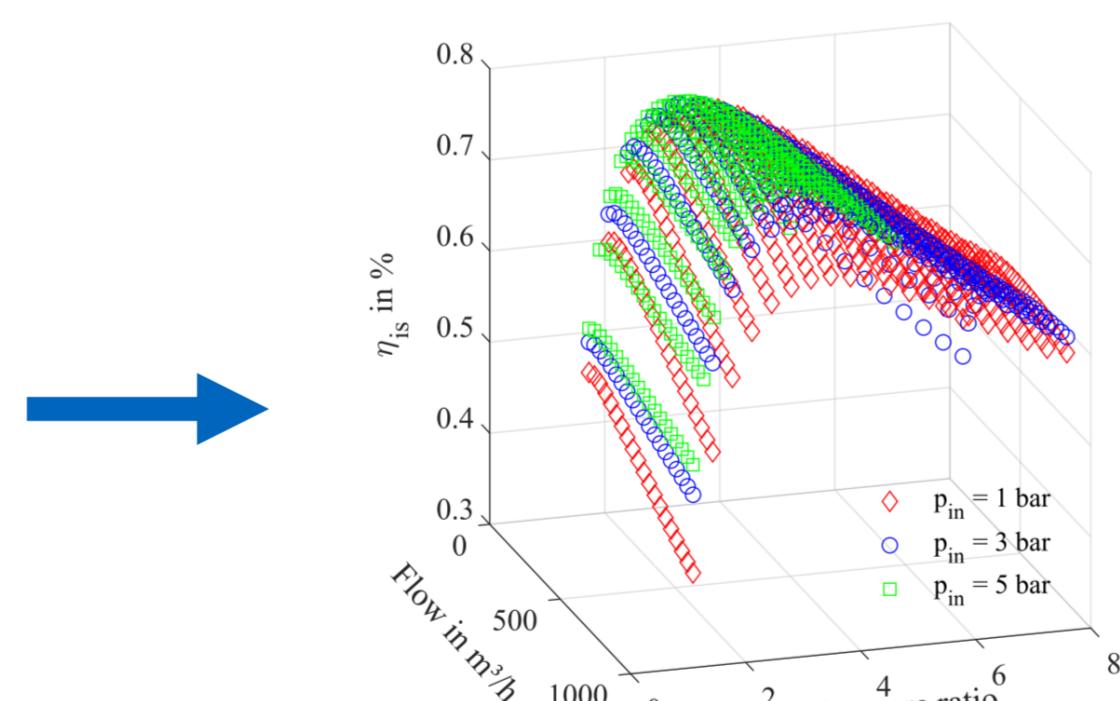


Figure 7: Performance map for the compressor simulation⁷

Research scope & evaluated concepts



Research Questions:

- I) Which compression heat pump configuration performs best under varying project conditions?
- II) How can the fluid selection for each stage further optimize the COP?
- III) Which LCOH can medium-deep geothermal projects achieve?

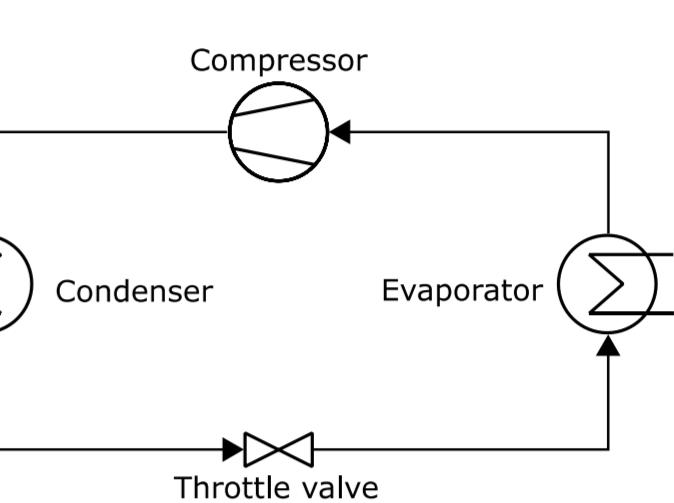


Figure 4: Single-stage compression heat pump

Single-stage HPs:

- + Lower CAPEX
- + Lower plant complexity
- Low COP; higher OPEX
- Strong off-design operation

$$COP_{Carnot} = 5.89$$

$$COP_{real} = 2.95$$

(50 % of the theoretical ideal performance)

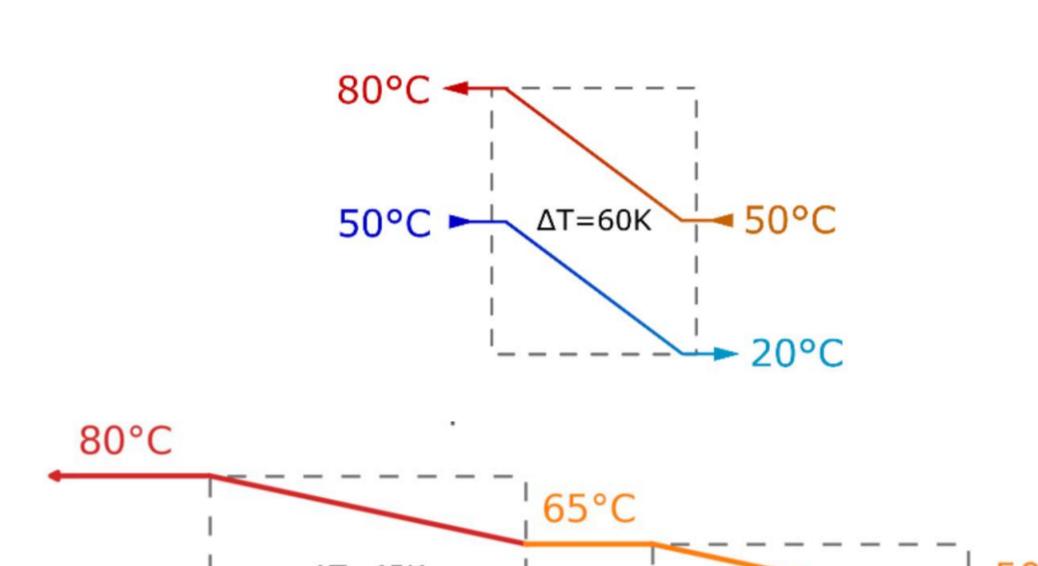


Figure 5: Distribution of temperature lift for different HP-concepts adapted from Mathes et al. (2022)⁴

Table 1: Key characteristics of some of the studied working fluids^{5,6}

Name	Type	p_{crit} [bar]	T_{crit} [°C]	Safety Group	GWP	ODP	PFAS issue?
Propane	Natural (HC)	42.5	96.7	A3	3	0	No
Butane	Natural (HC)	37.0	152.0	A3	4	0	No
Pentane	Natural (HC)	33.7	196.6	A3	10-20	0	No
Ammonia	Natural (NH ₃)	113.0	132.4	B2/B2L	0	0	No
R1224yf(Z)	HFO	33.4	155.5	A1	1	0.0002	Very high
R1233zd(E)	HFO	35.7	165.6	A1	1-4	0.0003	High

Economic Evaluation

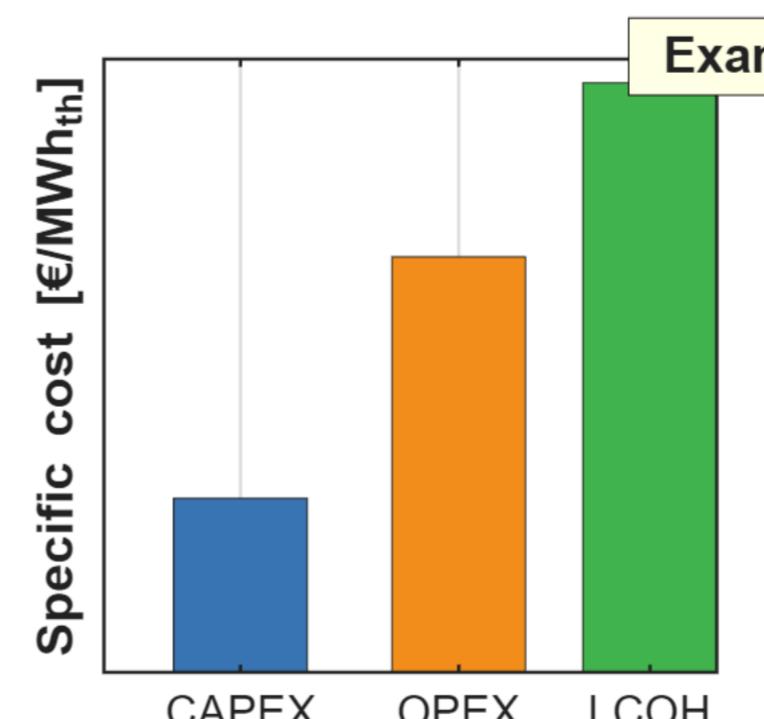


Figure 8: Conceptualization of the cost estimation method

Recommendation

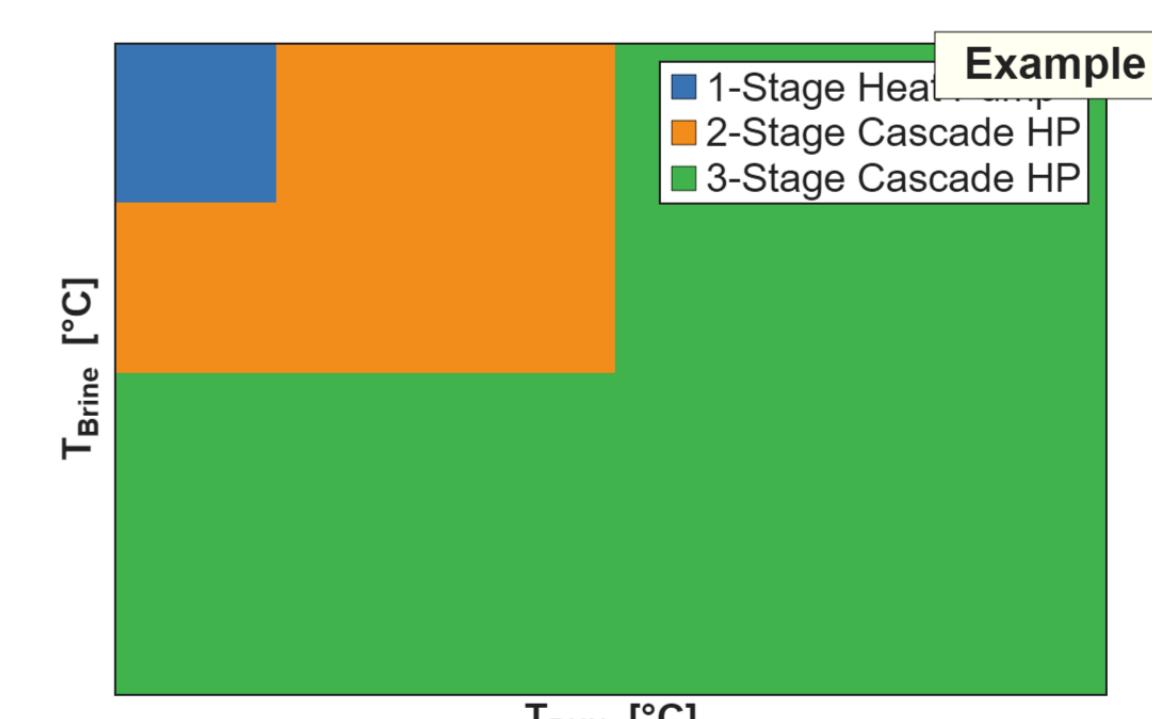


Figure 9: Conceptualization of the expected favourability map

- Using hourly demand data for realistic simulations
- Adapting the real data for various DHN and geothermal settings

- Simulating different HP concepts and compressor sizes
- Design optimization based on thermodynamic constraints and real operational behaviour

- Using output data of HP-simulation to calculate investment and operational costs as well as LCOH

- Determination of most favourable HP-setup based on geothermal conditions and DHN characteristic

